

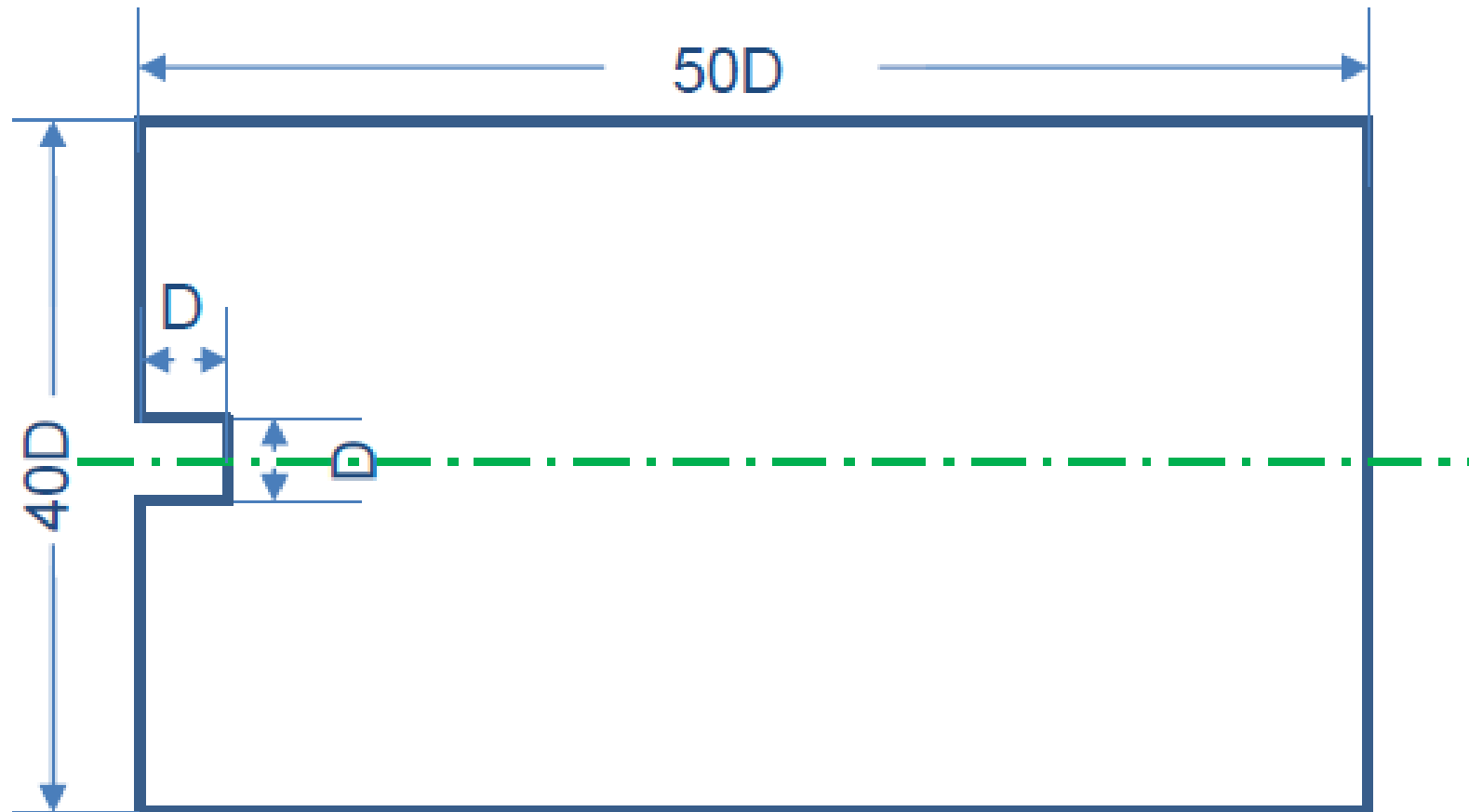
2D Jet Simulation Updates

Jan.23rd 2014

Yan Zhan

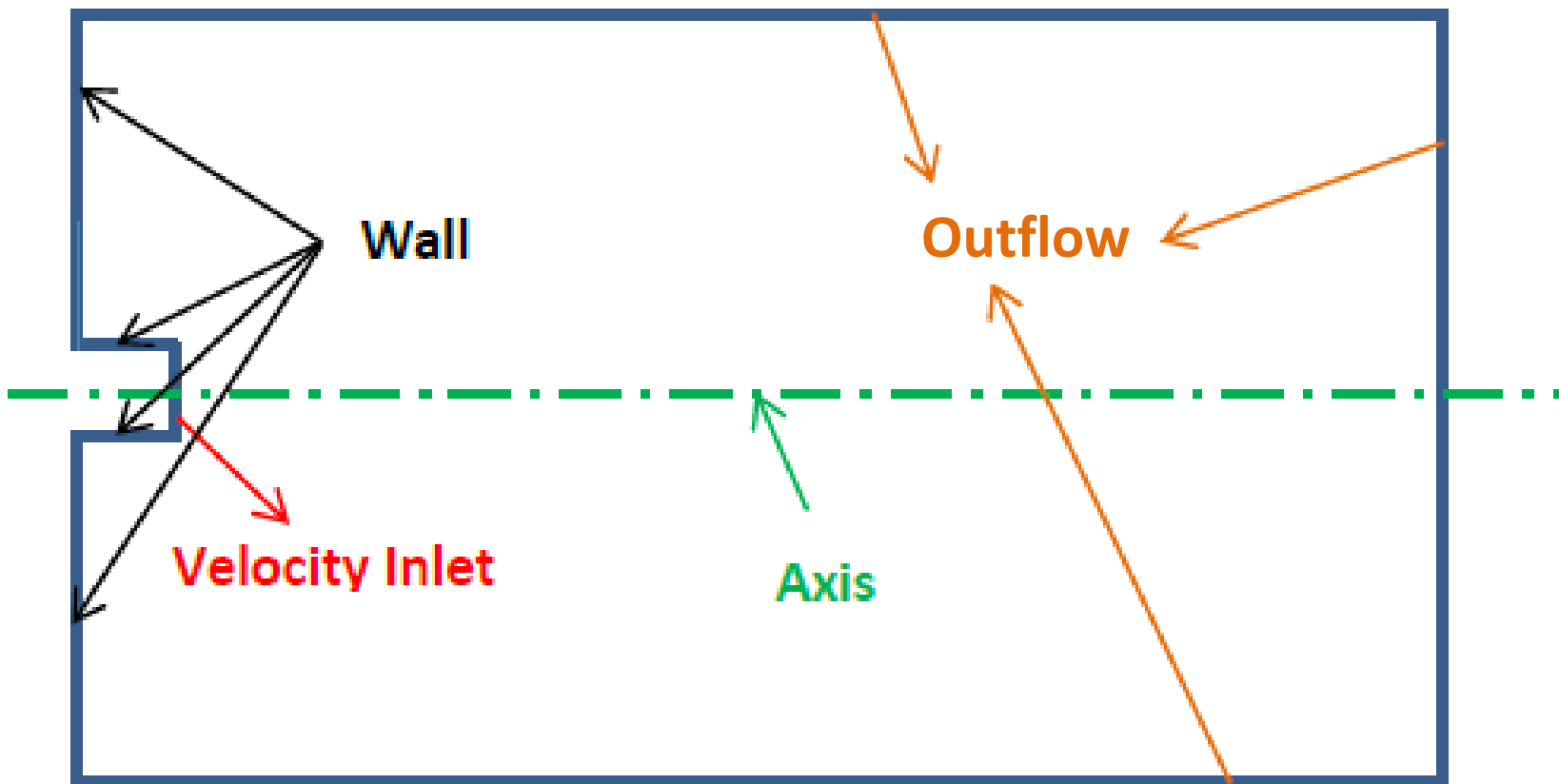
SUNY Stony Brook

Problem 1: Water-Air Jet



An axis-symmetric **water** jet into still **air** with a mean bulk velocity of **4.5455 m/s** ($D = 0.01\text{m}$, and $Re = 50,000$).

Boundary Conditions



Jet Characteristics

- Physical Characteristics

Diameter (D)	Velocity	Turbulent Intensity
0.0102108 m	4.5455 m/s	$u'/U = 0.05$

Phase	Density	Viscosity	Surface Tension
Air	1.225 kg/m ³	1.46×10^{-5} m ² /s	0.071 N/m
Water	998 kg/m ³	0.9×10^{-6} m ² /s	

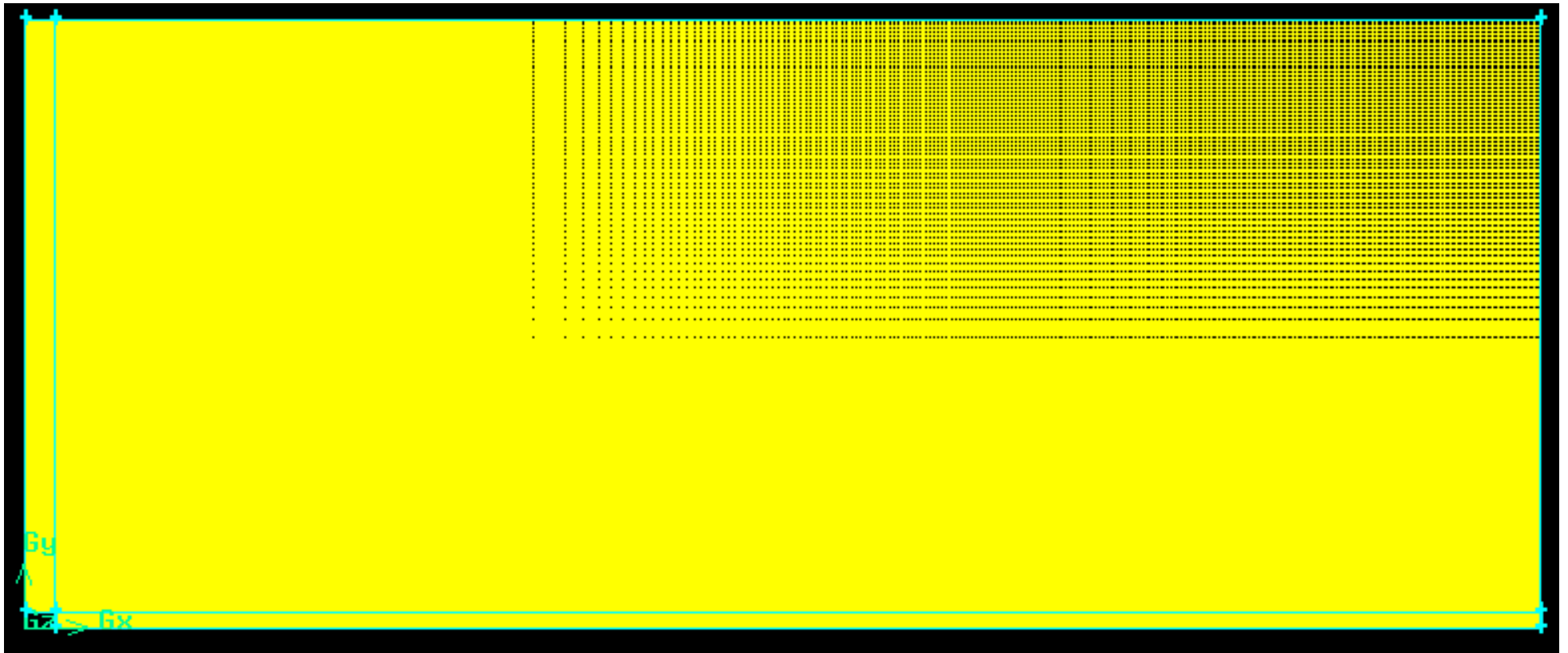
- Numerical Characteristics

- Determination of the mesh size:

Assume only primary breakup, the critical liquid Weber number is 10, then $\Delta x_{\text{critical}} = 34.4 \mu\text{m}$

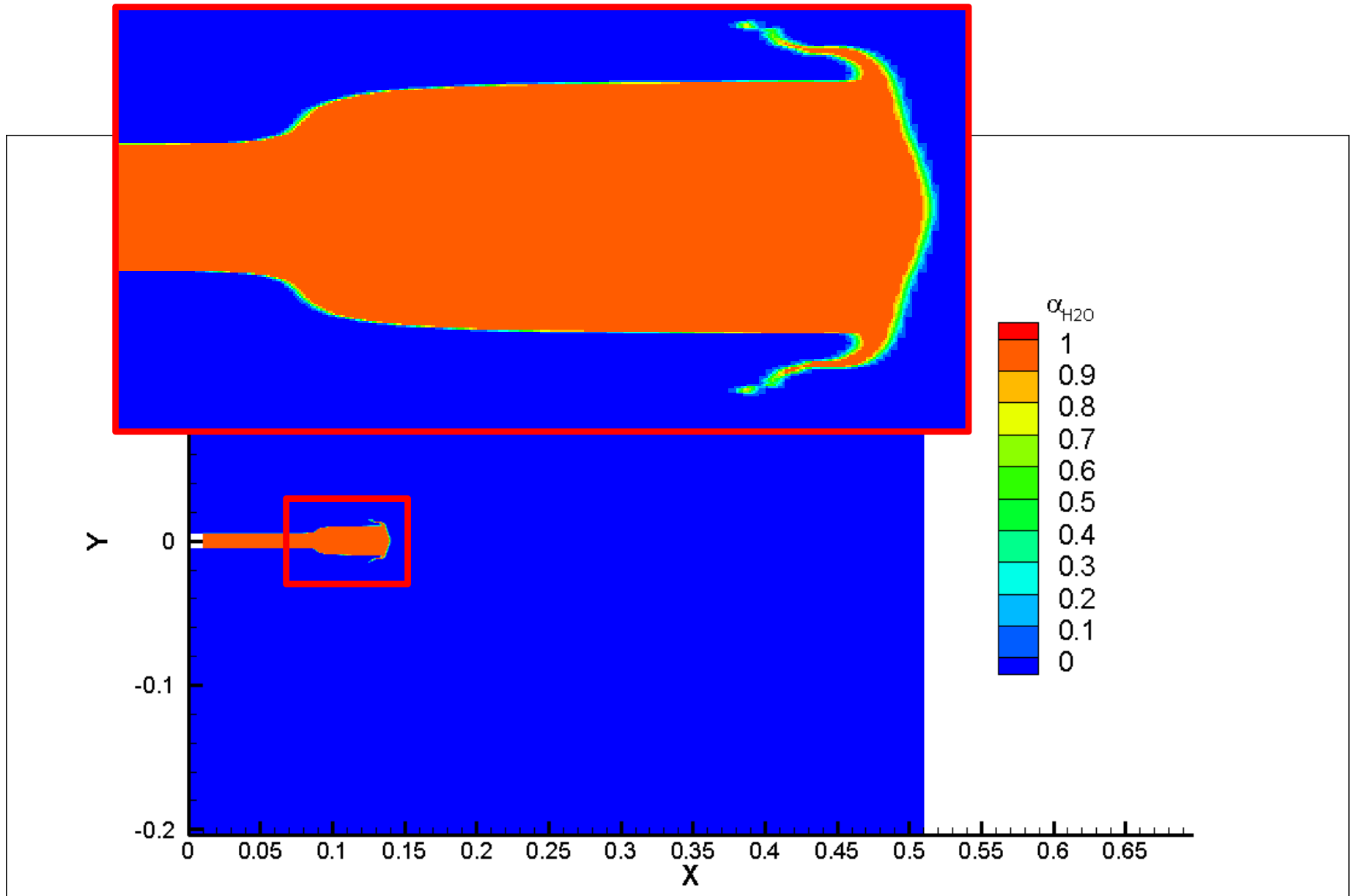
$$We \equiv \frac{\rho u^2 \Delta x}{\sigma} \rightarrow \Delta x = \frac{10 * 0.071}{998 * 4.5455 * 4.5455} = 3.44 * 10^{-5} \text{ m}$$

Mesh

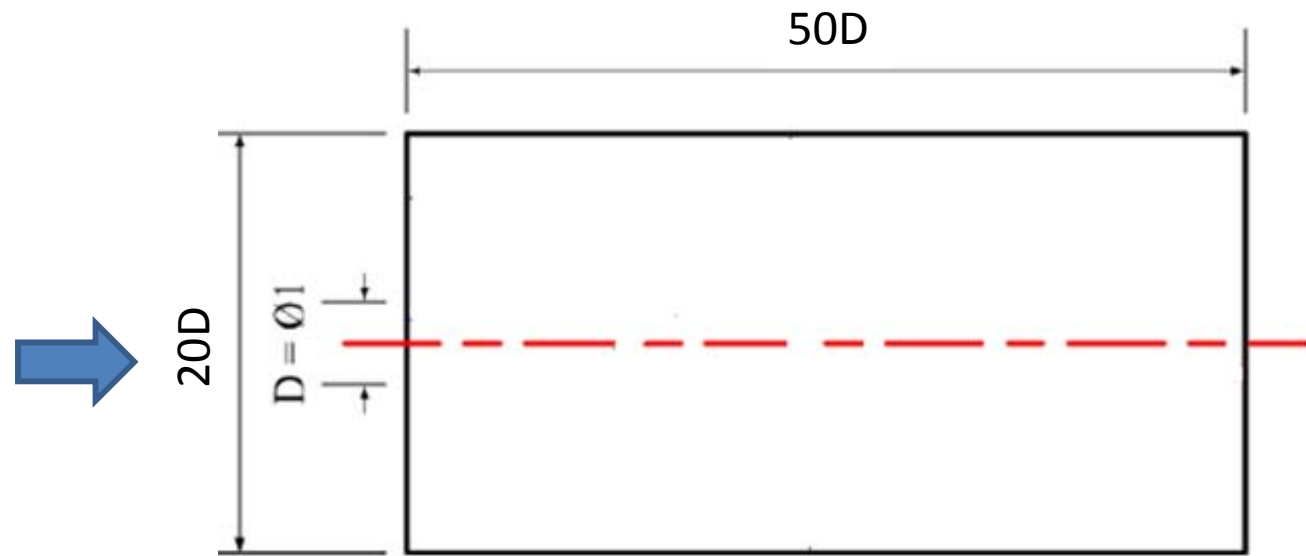
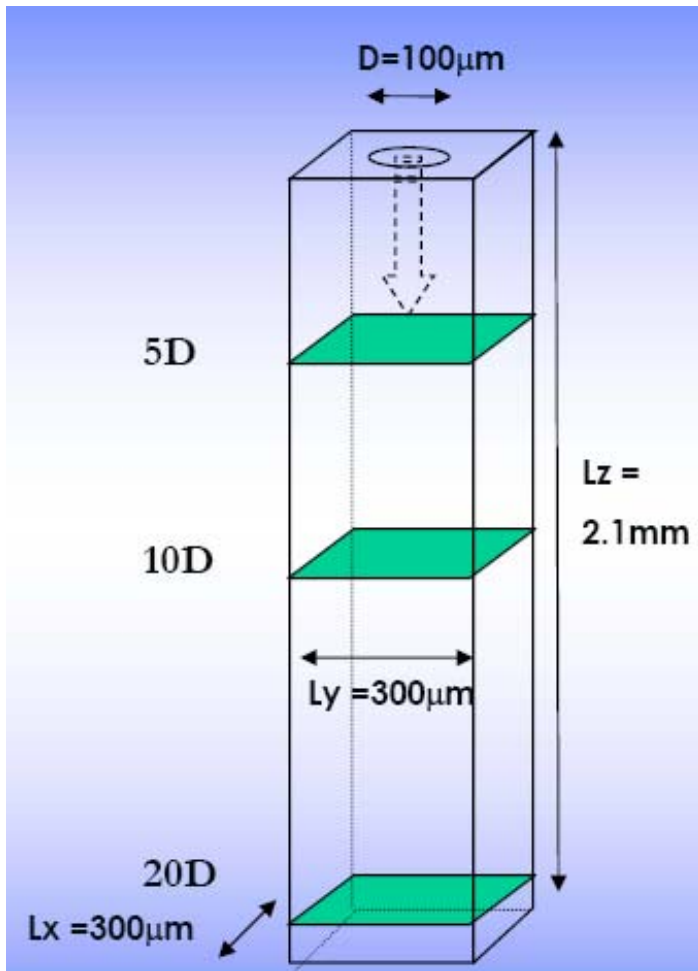


Halved (axis-symmetric) model with grid# of **822,000**

Results (t = 0.0307s)



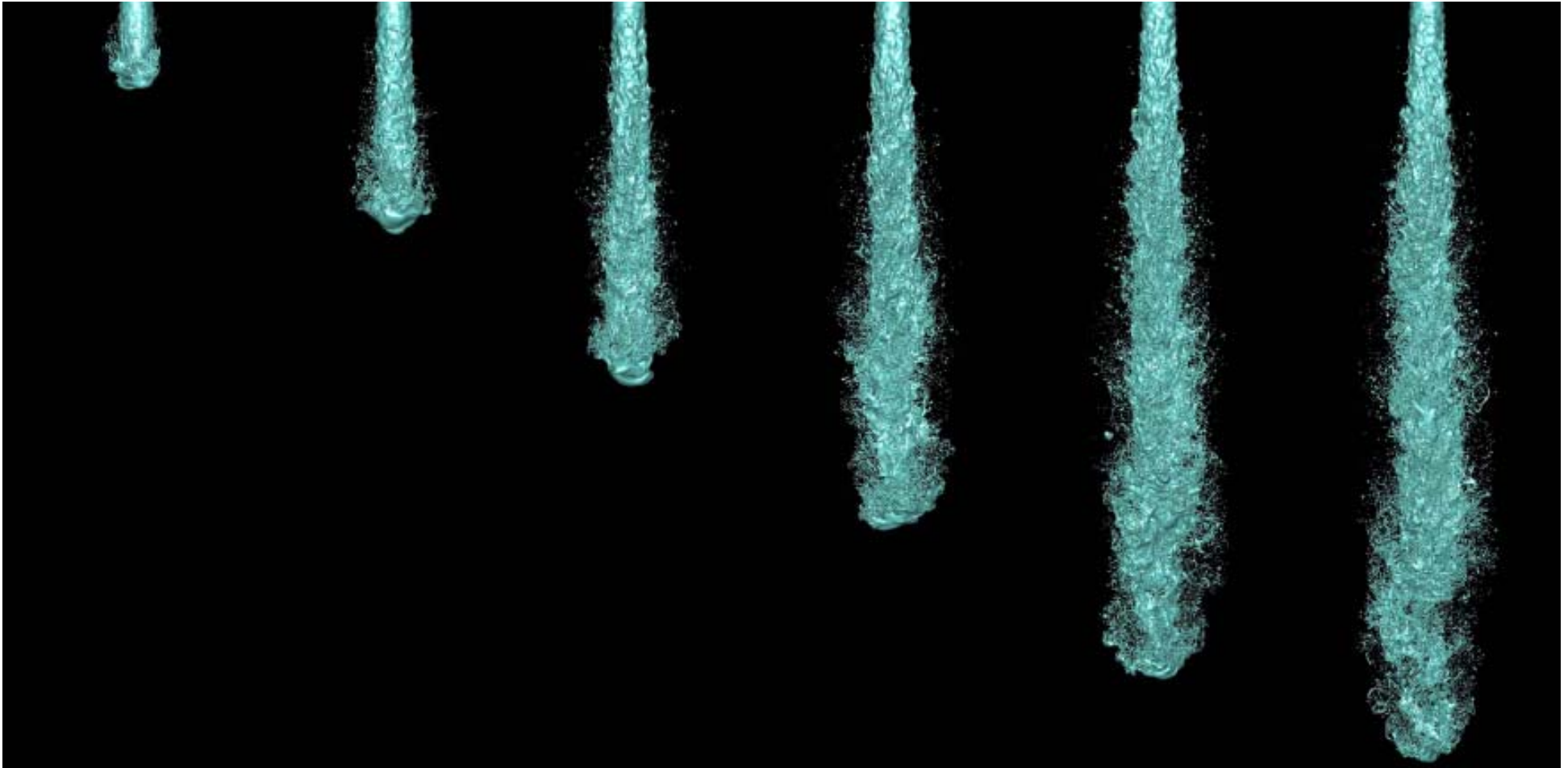
Problem 2: Menard's Test^[1]



An axis-symmetric **liquid** jet into still **gas** with a mean bulk velocity of **100 m/s** ($D = 100\ \mu\text{m}$, and $\text{Re} = 5,800$).

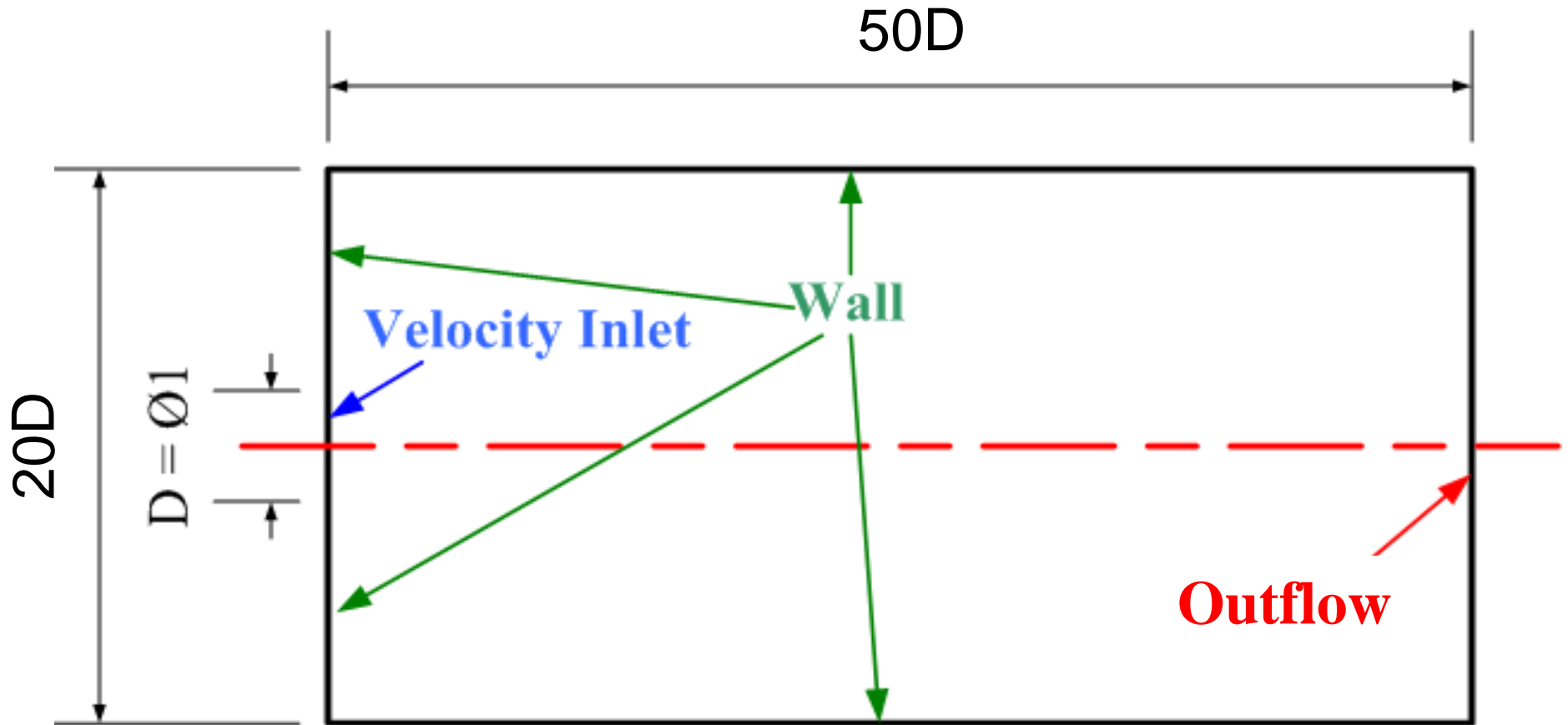
[1] T. Menard, etc., Coupling level set/VOF/ghost fluid methods: Validation and application to 3D simulation of the primary break-up of a liquid jet, International Journal of Multiphase Flow 33 (2007) 510–524

Menard's Results^[1]



Jet development and penetration ($dt = 2.5 \mu\text{m}$)

Boundary Condition



Jet Characteristics

- Physical Characteristics

Diameter (D)	Velocity	Turbulent Intensity
100 μm	100 m/s	$u'/U = 0.05$

Phase	Density	Viscosity	Surface Tension
Gas	25 kg/m ³	4×10^{-7} m ² /s	0.06 N/m
Liquid	696 kg/m ³	1.724×10^{-6} m ² /s	

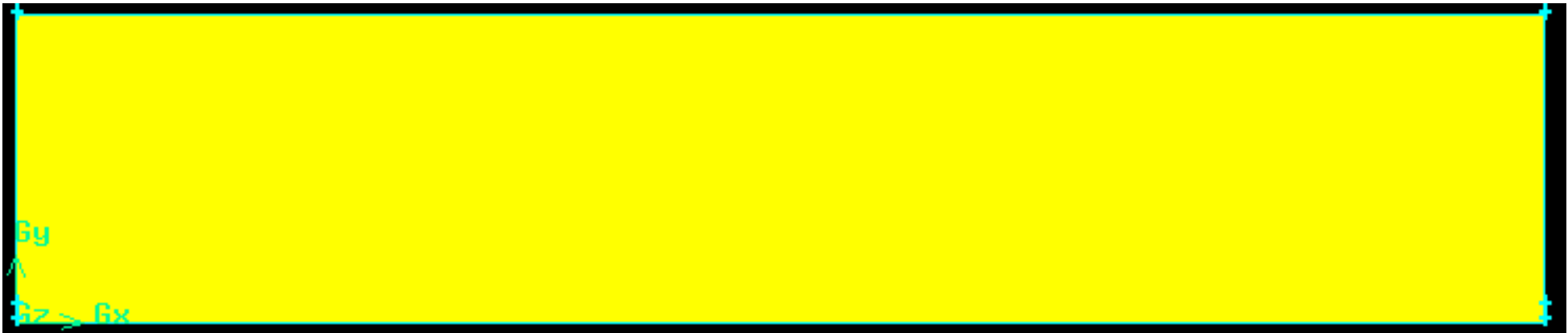
- Numerical Characteristics

- Determination of the mesh size:

Assume only primary breakup, the critical liquid Weber number is 10, then $\Delta x_{\text{critical}} = 2.36 \mu\text{m}$

$$We \equiv \frac{\rho u^2 \Delta x}{\sigma} \rightarrow \Delta x = \frac{10 * 0.06}{696 * 100 * 100} = 2.36 * 10^{-6} \text{ m}$$

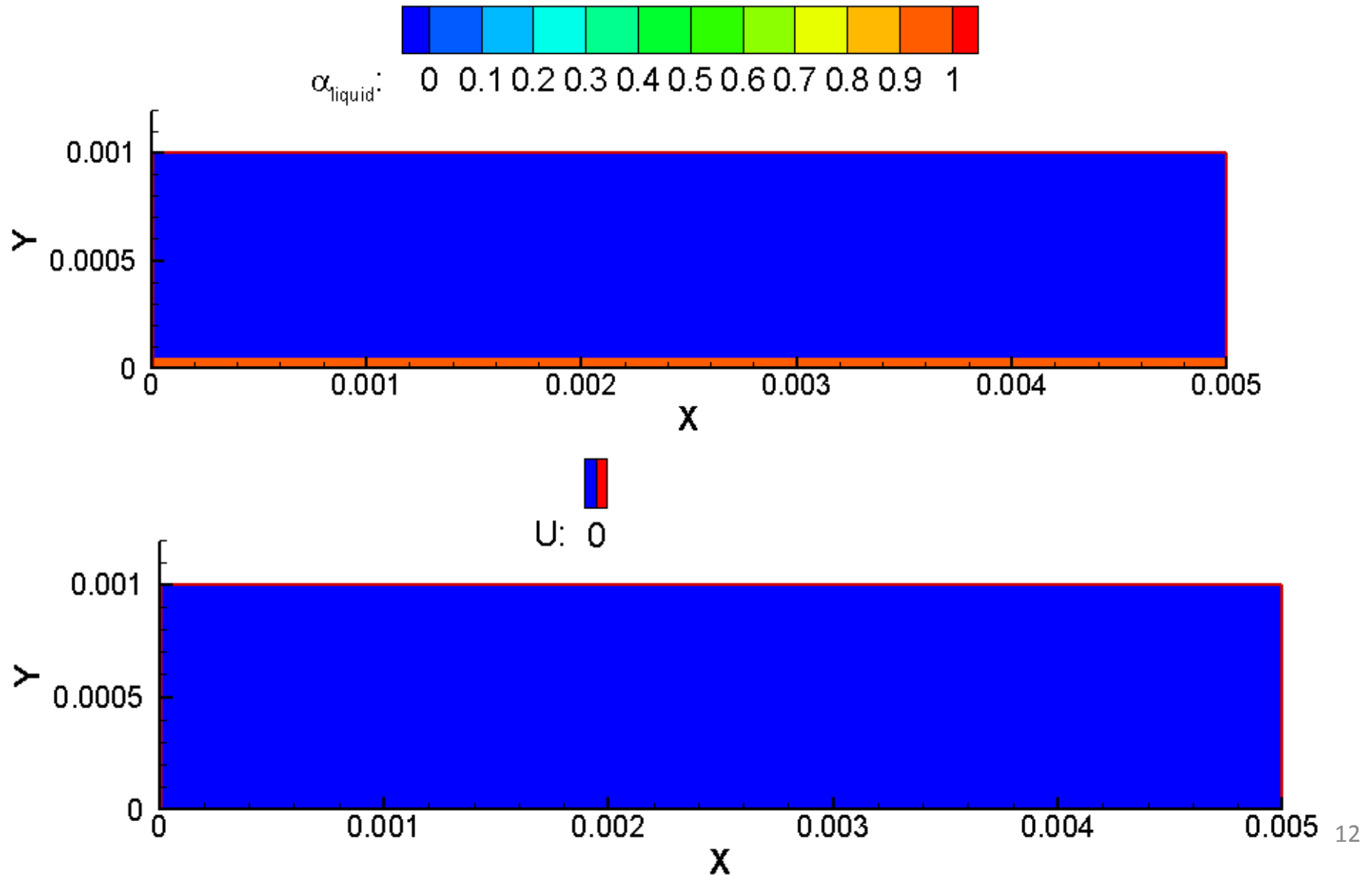
Mesh



Halved (axis-symmetric) model with grid# of **1,146,880**

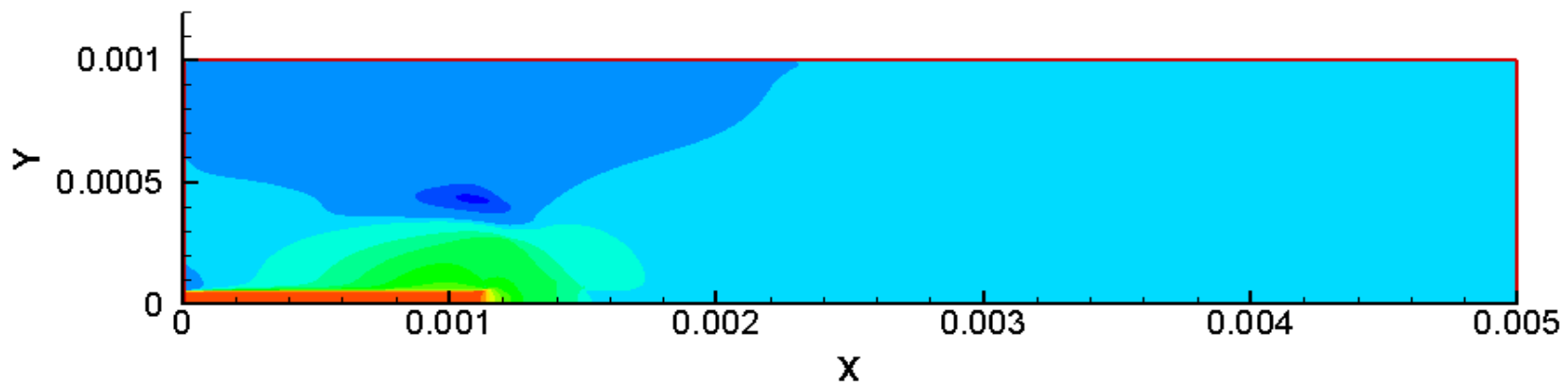
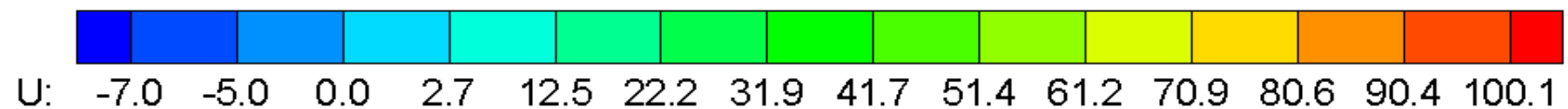
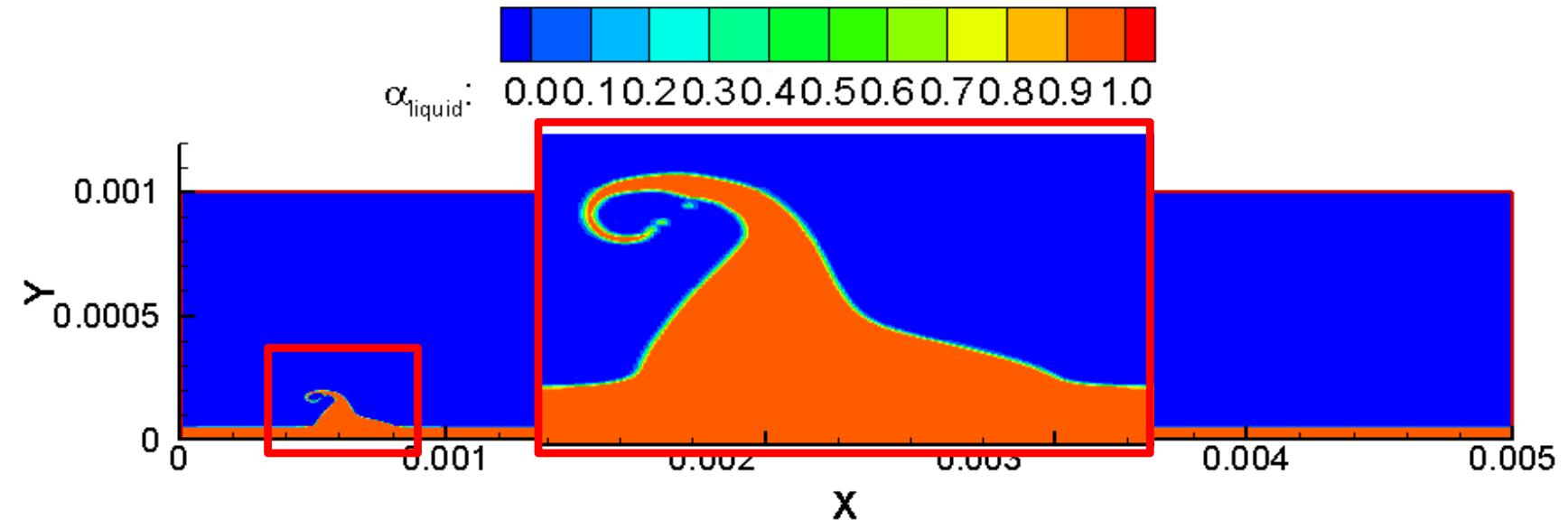
Results

- Set Up 1 (t = 0 s):



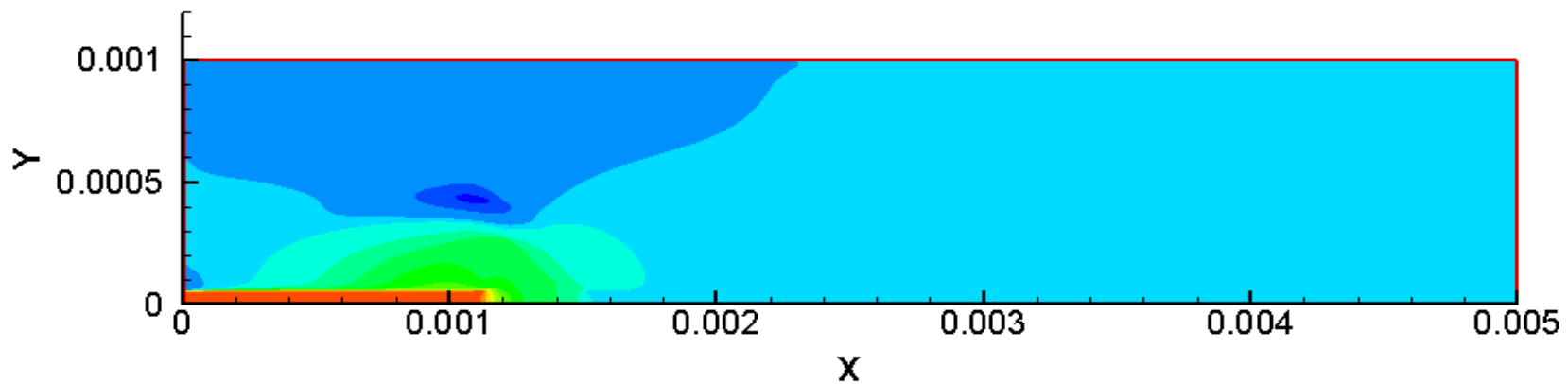
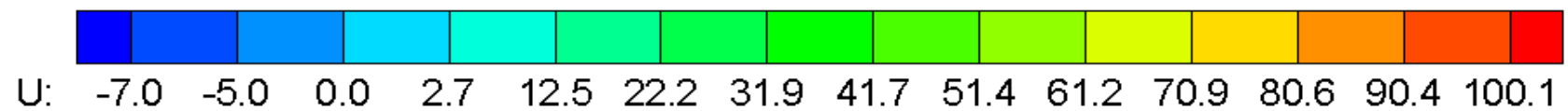
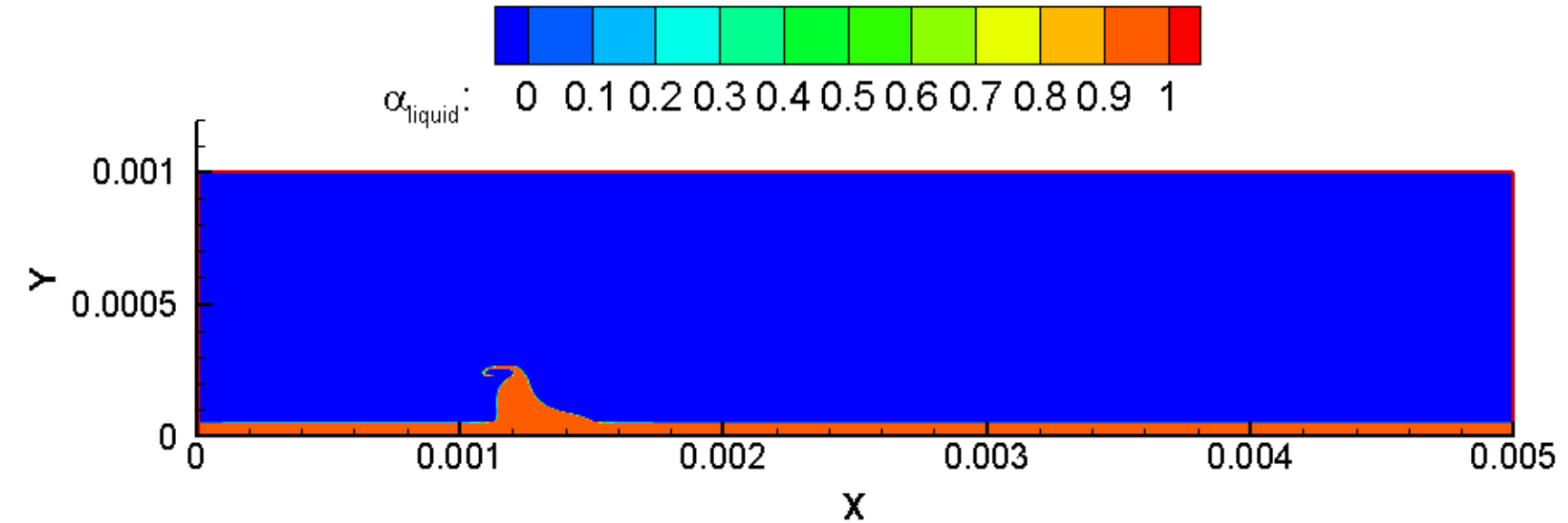
Results

- Set Up 1 ($t = 10 \mu\text{s}$):



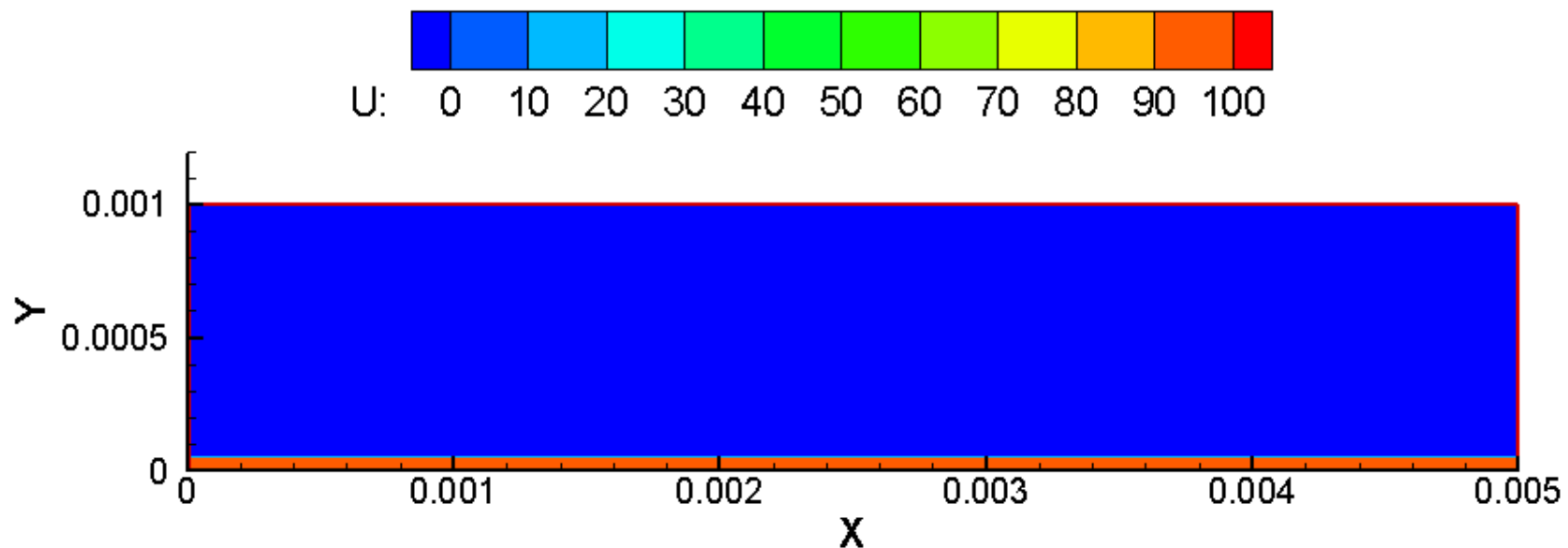
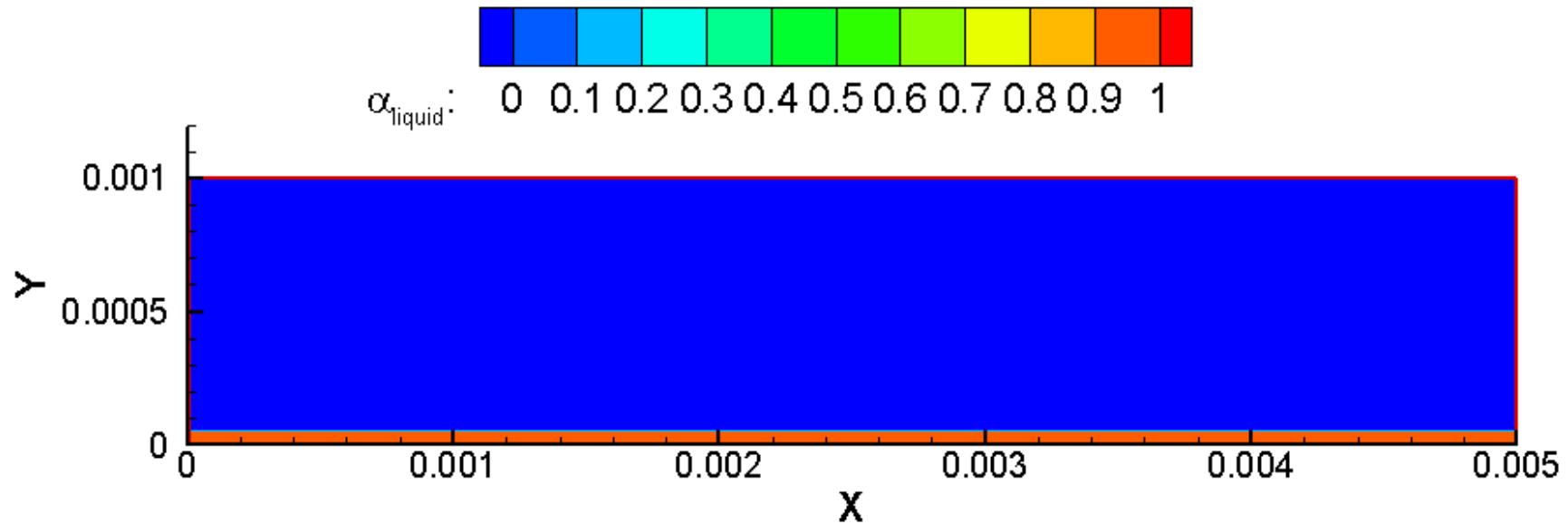
Results

- Set Up 1 ($t = 30 \mu\text{s}$):



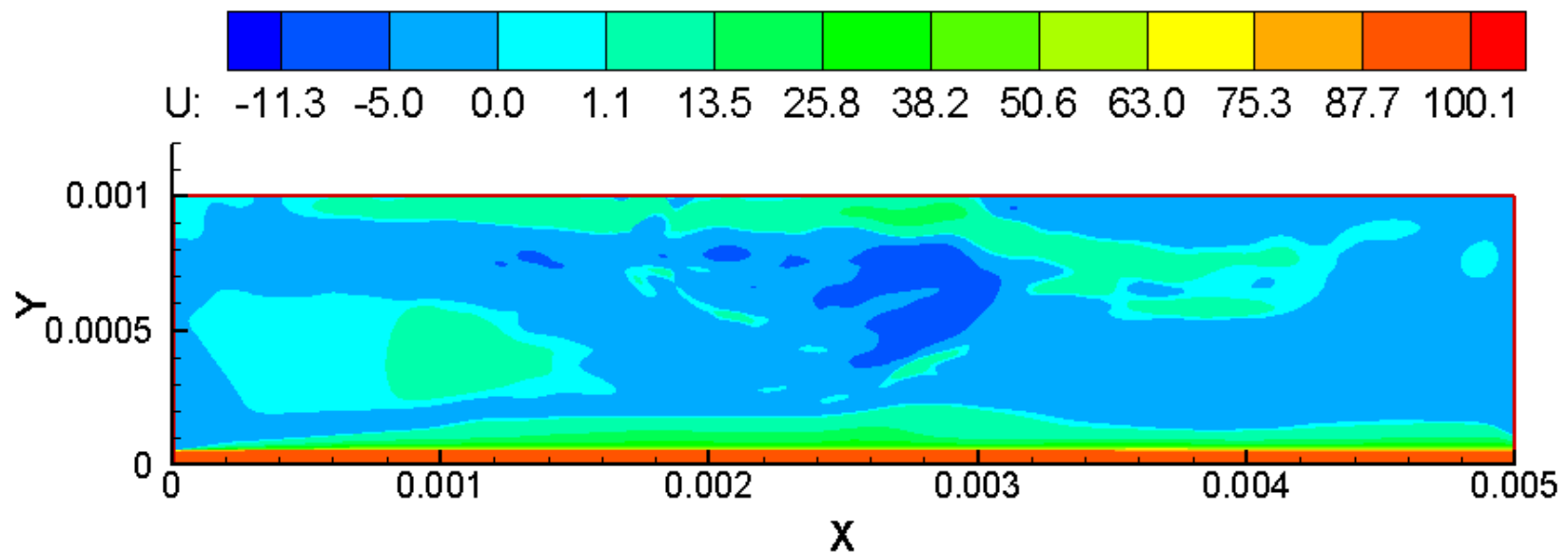
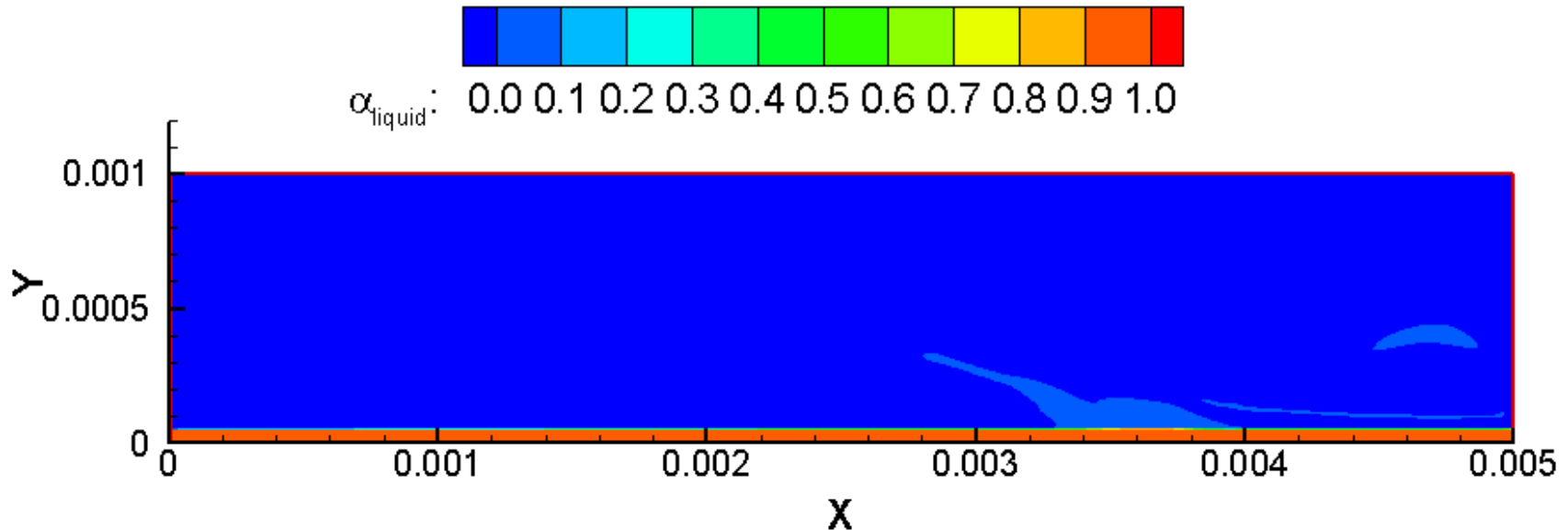
Results

- Set Up 2 (iteration = 0):



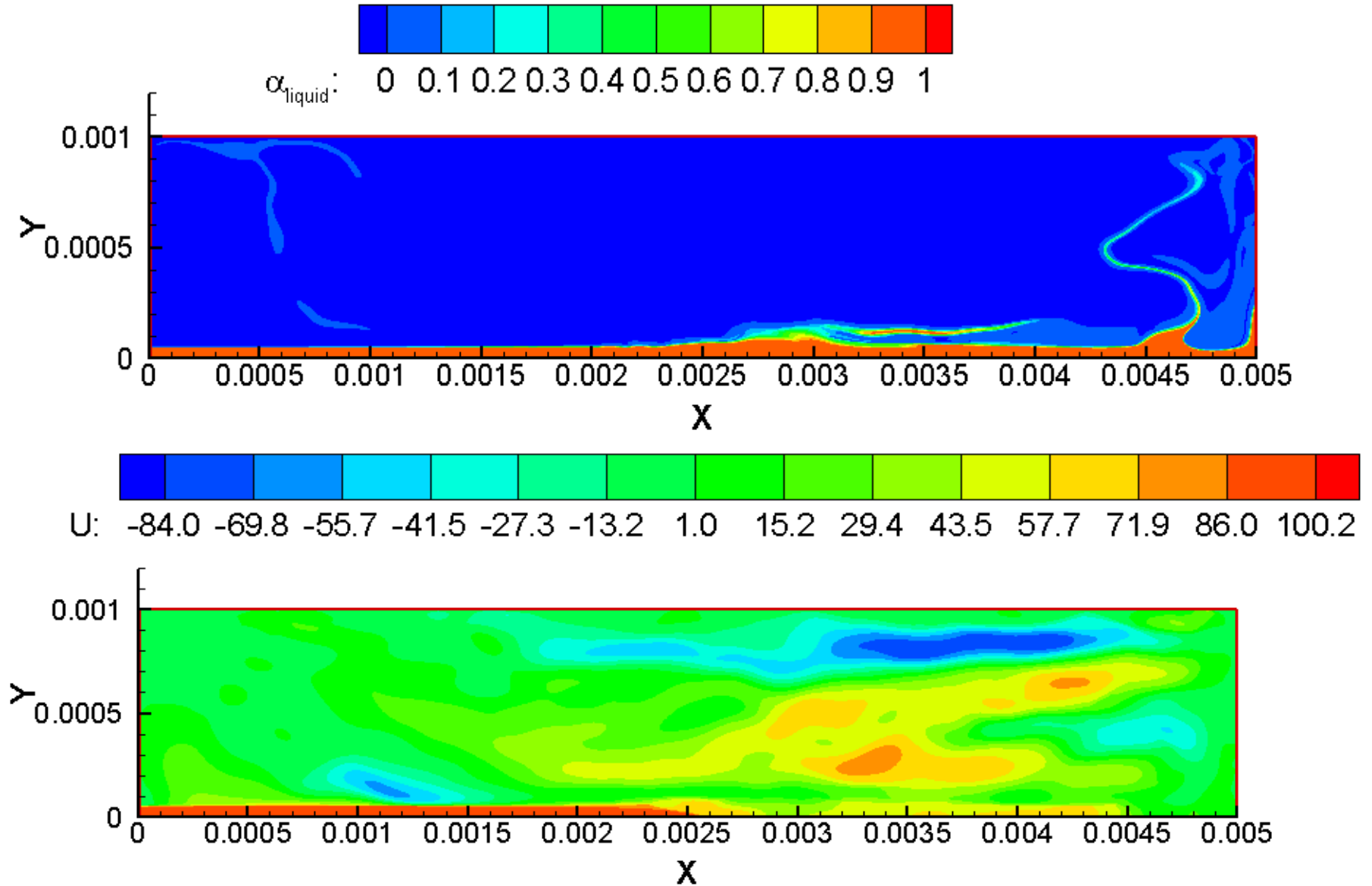
Results

- Set Up 2 (iteration = **1500**) : :



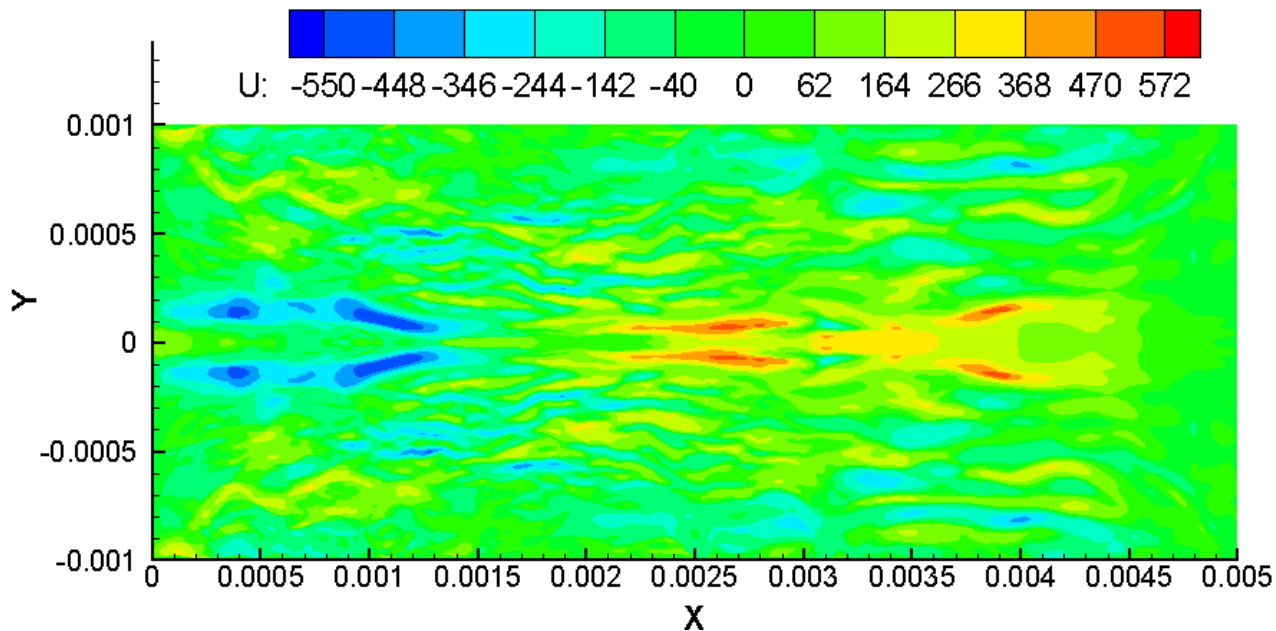
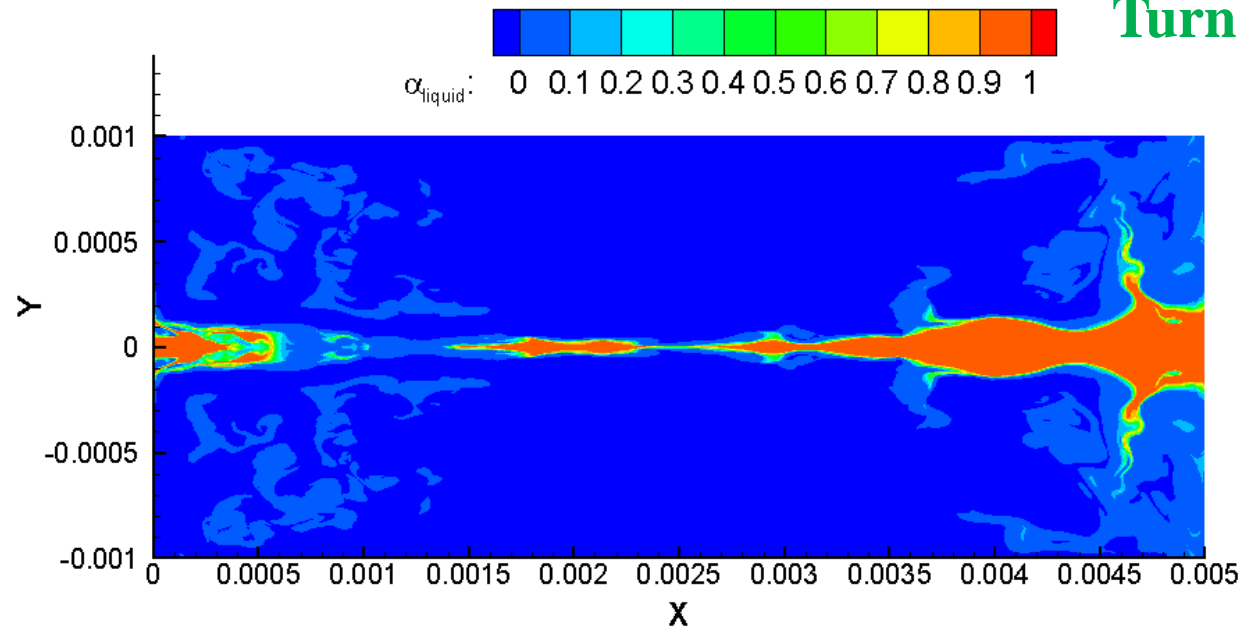
Results

- Set Up 2 (iteration = **3500**) :

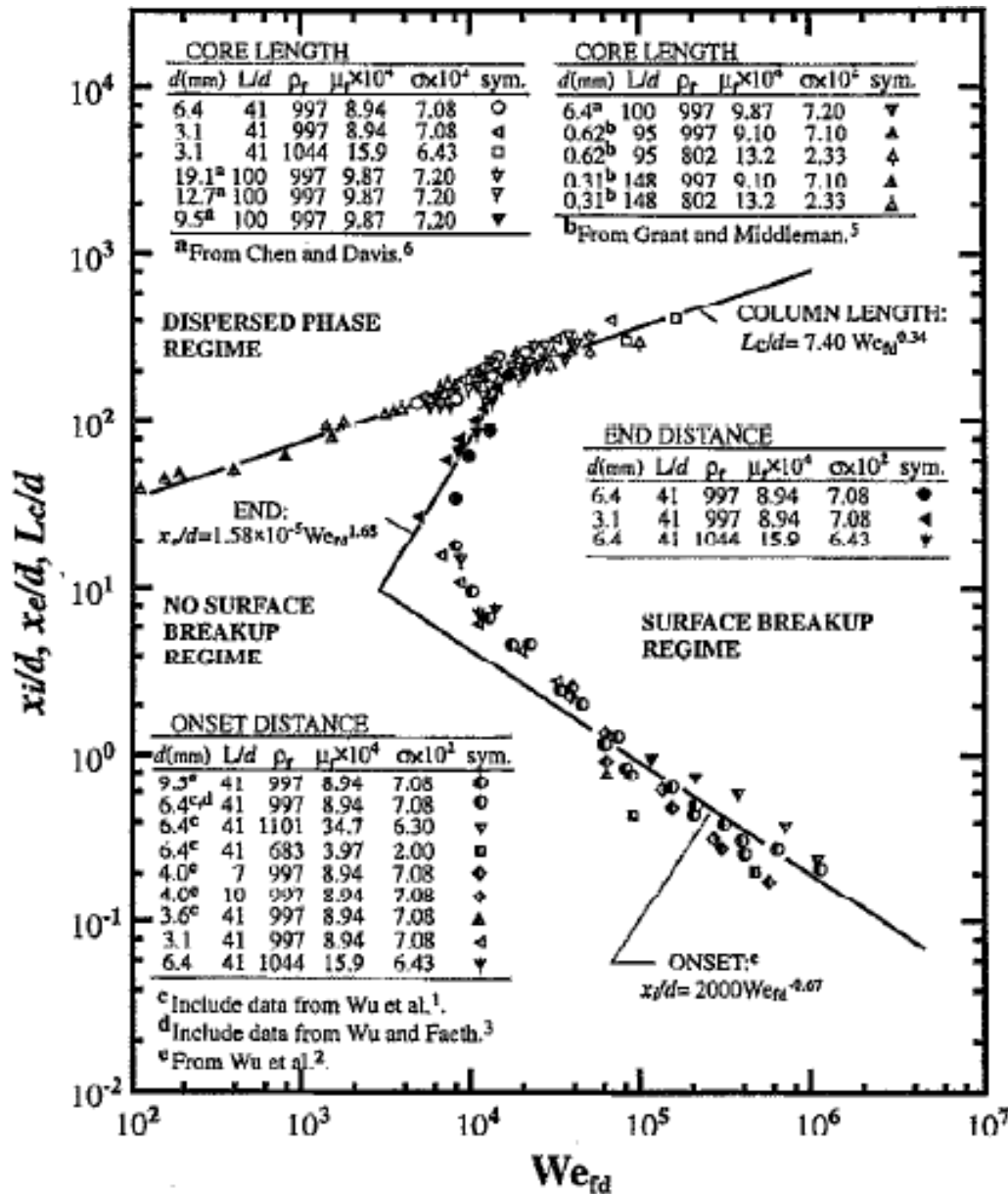


Results

- Set Up 2 (iteration = **4500**) : **Next:**
Turn to Unsteady Simulation



More Information



Considered Range:

Weber numbers ($We_{fd} = \rho d u_0^2 / \sigma$):
 $1.0 \times 10^2 - 1.1 \times 10^6$;

Reynolds numbers ($Re_{fd} = \rho_f d u_0 / \mu_f$):
 $3.4 \times 10^3 - 8.5 \times 10^5$;

Ohnesorge numbers ($Oh_d = \mu_f / \rho_f d \sigma$):
 $0.001 - 0.017$.

[2] P-K Wu and G M Faeth, Onset and end of drop formation along the surface of turbulent liquid jets in still gases, Phys. Fluids, Vol. 7, No. 11, November 1995

Surface breakup regime map for turbulent liquid jets in still gases when aerodynamic effects are small (liquid/gas density ratios are larger than 500)^[2]

More Information

Problem #	We_{fd}	Re_{fd}	OH_d	x_i $= 2000We_{fd}^{-0.67}d$	x_e $= 1.58 \times 10^{-5}We_{fd}^{1.68}d$
Problem 1	2,904	50,000	0.001	9.568d	10.387d
Problem 2	11,600	5,800	0.01857	3.783d	106.4d

x_i : location of onset of turbulent breakup;
 x_e : location of end of turbulent breakup.